# On Cavities in Thermally Spheroidized Powder Particles* 

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#### Abstract

A melted spherical particle begins to solidify on cooling, and the radius of the first thin solid layer is approximately equal to the radius of the melted particle. Since the density of the solid phase is higher than that of the liquid one, porosity forms inside the sphere during further solidification. The pressure in the remaining melted material may decrease considerably. The requirement for a pressure balance implies that a relationship for the pore radius can be derived. The pore arises as a bubble in a boiling liquid. The bubble stability and its minimum radius are derived, as well as conditions for its formation. It is shown that, at most, one bubble can occur in the particle. Analytical results are applied to the case of alumina particles, and the growing process of the cavity is simulated. Craters found on some spheroidized particles stem from asymmetry of the solid shell formation and the simultaneous action of the atmospheric pressure. The practical importance of this effect is that additional porosity may be formed in thermal spray products.


Keywords alumina powder, bubble formation in liquids, closed porosity, solidification of melted particles, thermally spheroidized powder

## 1. Introduction

Hollow spheres are often obtained during spheroidization of fine powder grains with the aid of, for example, plasma jets (Ref 1,2 ). Small cavities arise due to the higher density of the solidifying surface layer compared to the melted phase and when very fast cooling does not allow compression under atmospheric pressure (Ref 1).

The presence of cavities inside particles (see Fig. 1) leads to a lower density of the powder and, consequently, to additional porosity of the final products. Therefore, a more detailed analysis of that phenomenon may be desirable.

The purpose of this paper is to give a simple physical theory of cavity formation. Our study is based mostly on standard thermodynamics, with inhomogeneities connected with the crystal structures being neglected. Although this approach is not completely rigorous, it is used as a first approximation.

In what follows, the conditions to form cavities in quickly cooled solidifying particles are derived, possible motions of the cavities are pointed out, and the final volume of a cavity is calculated. The results are supported by a computer simulation of particle cooling and cavity growth.

## 2. Physical Model

### 2.1 Pressure Evolution in the Melted Phase

Assume a completely melted spherical particle with only radial dependence of temperature. If cooling of the particle is

[^0]spherically symmetric, a solid layer grows at the entire particle surface. Since the mass density of the solid phase, $\rho_{\mathrm{s}}$, is higher than the density of the melted one, $\rho_{\mathrm{m}}$, the hydrostatic pressure in the melted phase decreases. Simultaneously, the sphere radius, $R_{0}$, can decrease due to the atmospheric pressure. We assume that cooling is sufficiently fast that this sphere deformation is negligible. Thus, the radius $R_{0}$ of the first thin solid shell is constant.

Consider the pressure variations in the melted phase before formation of the cavity. Let $R_{\mathrm{m}}$ be the radius of the melted material, the layer between $R_{\mathrm{m}}$ and $R_{0}$ being solid. If the solidification steps by $\mid \Delta R_{m}!$ toward the sphere center, the remaining melted material is subjected to a volume dilatation of:

$$
\begin{equation*}
\Delta V_{\mathrm{p}}=\left(1-\frac{\rho_{\mathrm{m}}}{\rho_{\mathrm{s}}}\right) 4 \pi R_{\mathrm{m}}^{2}\left|\Delta R_{\mathrm{m}}\right|>0 \tag{Eq1}
\end{equation*}
$$

given by the increase of the mass density from $\rho_{m}$ to $\rho_{s}$ during the phase transition. The corresponding decrease of the pressure in the melted region is:

$$
\begin{equation*}
\Delta P=-\frac{\Delta V_{\mathrm{p}}}{\kappa V} \tag{Eq2}
\end{equation*}
$$

where K is the coefficient of the volume compressibility and $V$ is the volume of the melted phase. Using Eq 1 in Eq 2 and limiting $\Delta R_{\mathrm{m}} \rightarrow 0$, we obtain:

$$
\begin{equation*}
\frac{d P}{d R_{\mathrm{m}}}=\frac{3}{\kappa R_{\mathrm{m}}}\left(1-\frac{\rho_{\mathrm{m}}}{\rho_{\mathrm{s}}}\right) \tag{Eq3}
\end{equation*}
$$

a relation giving the dependence of the pressure in the whole melted region on its radius $R_{\mathrm{m}}$ :

$$
\begin{equation*}
P\left(R_{\mathrm{m}}\right)=P_{1}-\frac{3}{\kappa}\left(1-\frac{\rho_{\mathrm{m}}}{\rho_{\mathrm{s}}}\right) \ln \frac{R_{0}}{R_{\mathrm{m}}} \tag{Eq4}
\end{equation*}
$$

[^1]where $P_{1}$ is the atmospheric pressure (equal to initial pressure in the melted drop). Thermal dilatations different from $\Delta V_{\mathrm{p}}$ and possible variations of $\kappa$ have been neglected.

### 2.2 Bubble Formation

According to the Clausius-Clapeyron equation, the boiling point temperature decreases with pressure decrease. In fact, the pressure of the melted phase can even reach, for a moment, negative values at early stage of the solidification. Therefore, a bubble arises in the region of the highest temperature of the melt. If the radius of the (supposedly spherical) bubble is $R_{\mathrm{b}} \ll R_{\mathrm{m}}$, the pressure of the melted phase increases by:

$$
\begin{equation*}
\Delta P \simeq \frac{R_{\mathrm{b}}^{3}}{\mathrm{\kappa} R_{\mathrm{m}}^{3}} \tag{Eq5}
\end{equation*}
$$

Due to the surface tension, $\sigma$, the pressure inside the bubble is $2 \sigma / R_{\mathrm{b}}$ higher.

|  | Symbols |
| :--- | :--- |
| $\mathbf{F}$ | Force due to surface tension |
| $M$ | Molecular mass in atomic units |
| $P_{1}$ | Atmospheric pressure |
| $P_{\mathrm{v}}$ | Tension of vapors in the bubble |
| $\Delta P$ | Decrease of melted phase pressure |
| $q$ | Heat of evaporation |
| $R$ | Variable radius |
| $R_{0}$ | Radius of the initial droplet |
| $R_{\mathrm{b}}$ | Bubble radius |
| $R_{\mathrm{b}}^{\text {min }}$ | Minimum bubble radius |
| $R_{\mathrm{b} 1}$ | Radius of the unstable bubble |
| $R_{\mathrm{b} 2}$ | Radius of the stable bubble |
| $R_{\mathrm{c}}$ | Radius of the final cavity |
| $\mathrm{R}_{\mathrm{g}}$ | Universal gas constant |
| $R_{\mathrm{m}}$ | Radius of the melted material |
| $\Delta R_{\mathrm{atm}}$ | Particle radius decrease owing to the |
| $\Delta R_{\mathrm{m}}$ | atmospheric pressure |
| $\Delta R_{\mathrm{s}}$ | Solidification step toward the sphere center |
| $\Delta V_{\mathrm{p}}$ | Melted material dilatation due to $\Delta R_{\mathrm{m}}$ |
| $T$ | Local temperature in the melted phase |
| $T_{1}$ | Boiling point temperature at $P_{1}$ |
| $T_{\mathrm{b}}$ | Temperature in the bubble |
| $T_{\mathrm{cr}}$ | Critical temperature |
| $T_{\mathrm{m}}$ | Melting point temperature |
| $T_{\mathrm{max}}$ | Maximum temperature in the melted material |
| $V$ | Volume of the melted phase |
| $V_{0}$ | Volume of the initial droplet |
| $V$ | Volume of the final cavity |
| $V_{\mathrm{ce}}$ | Experimentally found cavity volume |
| $\alpha_{\mathrm{v}}$ | Coefficient of thermal volume dilatation |
| $\kappa$ | Coefficient of volume compressibility |
| $\mu$ | Viscosity of the melted material |
| $\rho_{\mathrm{m}}$ | Density of the melted phase |
| $\rho_{\mathrm{s}}$ | Density of the solid phase |
| $\sigma$ | Surface tension |
|  |  |
|  |  |

Let us introduce the thickness of the solid shell, $\Delta R_{\mathrm{s}}=R_{0}-$ $R_{\mathrm{m}}$. Accounting for only first-order terms $\Delta R_{\mathrm{s}} / R_{0}$ in Eq 4 and neglecting them in Eq 5 , we obtain the equation of pressure equilibrium in the bubble as:

$$
\begin{equation*}
P_{\mathrm{v}}-P_{1}+\frac{3}{\kappa}\left(1-\frac{\rho_{\mathrm{m}}}{\rho_{\mathrm{s}}}\right) \frac{\Delta R_{\mathrm{s}}}{R_{0}}=\frac{R_{\mathrm{b}}^{3}}{\kappa R_{0}^{3}}+\frac{2 \sigma}{R_{\mathrm{b}}} \tag{Eq6}
\end{equation*}
$$

where $P_{\mathrm{v}}$ is the tension of vapors in the bubble, $P_{\mathrm{v}}<P_{1} . P_{\mathrm{v}}$ could be found from the data given in Ref 3, or determined approximately from the relation:

$$
\begin{equation*}
P_{\mathrm{v}} \simeq P_{1} \exp \left[\frac{g}{\mathrm{R}_{\mathrm{g}}}\left(\frac{1}{T_{1}}-\frac{1}{T_{\mathrm{b}}}\right)\right] \tag{Eq7}
\end{equation*}
$$

where $q$ is the heat of evaporation, $\mathrm{R}_{\mathrm{g}}$ is the universal gas constant, $T_{1}$ is the boiling point temperature at the atmospheric pressure $P_{1}$, and $T_{\mathrm{b}}$ is the temperature in the bubble. Considerable discrepancies have been found in the literature concerning the $q$ and $P_{\mathrm{v}}$ values in the case of $\mathrm{Al}_{2} \mathrm{O}_{3}$. However, useful information can be extracted from Eq 6 without determining the value of $P_{\mathrm{v}}$. Note that the left-hand side of the equation increases linearly with $\Delta R_{\mathrm{s}}$ from a negative value at $\Delta R_{\mathrm{s}}=0$. The right-hand side of Eq 6 is positive for all values of the bubble radius $R_{\mathrm{b}}$. The algebra of this expression implies that:

- At a given $\Delta R_{\mathrm{s}}$, two real values, $R_{\mathrm{b} 1}$ and $R_{\mathrm{b} 2}\left(R_{\mathrm{b} 1} \leq R_{\mathrm{b} 2}\right)$, satisfy Eq 6 .
- The right-hand side of Eq 6 as a function of $R_{\mathrm{b}}$ has a single minimum at:

$$
\begin{equation*}
R_{\mathrm{b}}^{\min }=R_{0}\left(\frac{2 \sigma \kappa}{3 R_{0}}\right)^{1 / 4} \tag{Eq8}
\end{equation*}
$$

Note that this value does not depend on $\rho_{\mathrm{s}}$ and $\rho_{\mathrm{m}}$.

- The minor root $R_{\mathrm{b} 1} \leq R_{\mathrm{b}}^{\text {min }}$ is unstable.
- Therefore, the stable solution of Eq 6 is:

$$
\begin{equation*}
R_{\mathrm{b}}=R_{\mathrm{b} 2}>R_{\mathrm{b}}^{\min } \tag{Eq9}
\end{equation*}
$$

The minimum value of the right-hand side of Eq 6 (multiplied by $\kappa$ ) corresponding to the value of $R_{\mathrm{b}}^{\mathrm{min}}$ is approximately:

$$
\frac{7}{4}\left(\frac{2 \sigma \kappa}{R_{0}}\right)^{3 / 4}
$$

Thus, the solution of Eq 6 exists if:

$$
\begin{equation*}
\kappa\left(P_{\mathrm{v}}-P_{1}\right)+3\left(1-\frac{\rho_{\mathrm{m}}}{\rho_{\mathrm{s}}}\right) \frac{\Delta R_{\mathrm{s}}}{R_{0}} \geq \frac{7}{4}\left(\frac{2 \sigma \kappa}{R_{0}}\right)^{3 / 4} \tag{Eq10}
\end{equation*}
$$

In other words, this inequality is the condition of existence of the stable bubble. Since $P_{\mathrm{v}}<P_{1}$, the necessary condition for this is:

$$
\begin{equation*}
\frac{\Delta R_{\mathrm{s}}}{R_{0}} \geq \frac{7}{12}\left(\frac{2 \sigma \kappa}{R_{0}}\right)^{3 / 4}\left(1-\frac{\rho_{\mathrm{m}}}{\rho_{\mathrm{s}}}\right)^{-1} \tag{Eq11}
\end{equation*}
$$

On the other hand, the sufficient condition for the existence of the bubble is obtained by deleting the unknown value of $P_{\mathrm{v}}$ :

$$
\begin{equation*}
\frac{\Delta R_{\mathrm{s}}}{R_{0}} \geq \frac{1}{3}\left(1-\frac{\rho_{\mathrm{m}}}{\rho_{\mathrm{s}}}\right)^{-1}\left[\frac{7}{4}\left(\frac{2 \sigma \kappa}{R_{0}}\right)^{3 / 4}+\kappa P_{1}\right] \tag{Eq12}
\end{equation*}
$$

These relations are used in section 3 for practical estimates.

### 2.3 Bubble Motion in Temperature Gradient

Surface tension, $\sigma$, decreases with increasing temperature, $T$ (Ref 3):

$$
\begin{equation*}
\frac{d \sigma}{d T}=-B\left(\frac{\rho_{\mathrm{m}}}{M}\right)^{2 / 3} \tag{Eq13}
\end{equation*}
$$

where $M$ is the molecular mass in atomic units and $B=2.1 \times$ $10^{-5} \mathrm{~kg}^{1 / 3} \mathrm{~m}^{2} \mathrm{~s}^{-2} \mathrm{~K}^{-1}$. If the temperature in the vicinity of the bubble is inhomogeneous, the pressure $2 \sigma / R_{\mathrm{b}}$ is also inhomogeneous. Assuming that, near the bubble, the temperature changes slightly with respect to the bubble diameter, we integrate the pressure $2 \sigma / R_{\mathrm{b}}$ over the bubble surface to obtain the net force acting on the bubble:

$$
\begin{equation*}
\mathbf{F} \simeq-\frac{8}{3} \pi R_{\mathrm{b}}^{2} \frac{d \sigma}{d T} \operatorname{grad} T \tag{Eq14}
\end{equation*}
$$

In other words, the force $-\mathbf{F}$ acts on the liquid adjacent to the bubble. Consequently, the bubble moves with velocity $\mathbf{v}$, given by the balance of the force $\mathbf{F}$ and the viscous drag $(\operatorname{Ref} 4)$ :

$$
\begin{equation*}
\mathbf{v} \simeq-\frac{2 R_{\mathrm{b}}}{3 \mu} \frac{d \sigma}{d T} \operatorname{grad} T \tag{Eq15}
\end{equation*}
$$

where $\mu$ is the viscosity of the melted material. As a result, a bubble born in a region of inhomogeneous temperature will move toward the temperature maximum.

### 2.4 Volume of the Final Cavity

Concluding this section, we present an expression for the volume, $V_{c}$, of the resulting cavity in the solidified spherical drop. According to our idealized model of zero deformation by atmospheric pressure, $V_{c}$ equates to the difference between the volumes of the melted and solid matter. This is calculated by considering the inverse process, namely, melting of the solid particle. In this case, unlike the previous discussion, the thermal dilatation of the melted drop is included. Integration over the volume, $V_{0}$, of the spheric drop gives:

$$
\begin{equation*}
\frac{V_{\mathrm{c}}}{V_{0}} \simeq 1-\frac{\rho_{\mathrm{m}}}{\rho_{\mathrm{s}}}+\frac{3 \alpha_{\mathrm{v}}}{R_{0}^{3}} \int_{0}^{R_{0}}\left[T(R)-T_{\mathrm{m}}\right] R^{2} d R \tag{Eq16}
\end{equation*}
$$

where $\alpha_{v}$ is the coefficient of thermal volume dilatation, $T_{\mathrm{m}}$ is the melting point temperature, and $T(R)$ is the local temperature at the moment of the sphere surface solidification. The last term in Eq 16 is often negligible. Then,

$$
\begin{equation*}
\frac{R_{\mathrm{c}}}{R_{0}} \simeq\left(1-\frac{\rho_{\mathrm{m}}}{\rho_{\mathrm{s}}}\right)^{1 / 3} \tag{Eq17}
\end{equation*}
$$

is a simple estimate of the cavity radius $R_{\mathrm{c}}$.

## 3. Estimates for Alumina Particles

The mass densities of melted and solid $\mathrm{Al}_{2} \mathrm{O}_{3}$ are $\rho_{\mathrm{m}}=2750$ $\mathrm{kg} / \mathrm{m}^{3}$ and $\rho_{\mathrm{s}}=3900 \mathrm{~kg} / \mathrm{m}^{3}$. The value of the surface tension is estimated by using Eq 13 , where now $M=102$ :

$$
\begin{equation*}
\frac{d \sigma}{d T} \simeq-1.9 \times 10^{-4} \mathrm{~N} / \mathrm{mK} \tag{Eq18}
\end{equation*}
$$

This is integrated from the critical temperature, $T_{\mathrm{cr}}$, where $\sigma=0$, to the maximum temperature, $T_{\max }$, in the melted phase. According to Ref 3 , a rough estimate is $T_{\text {cr }} \simeq T_{1} / 0.64, T_{1} \doteq 3000^{\circ} \mathrm{C}$, and, therefore, $T_{\mathrm{cr}} \simeq 4700^{\circ} \mathrm{C}$.

The value of $T_{\text {max }}$ is given by numerical modeling that is based on improving the finite-element method used in Ref 5 to model the thermal evolution of alumina particles in a plasma jet. The improvement takes into account the volume changes due to solidification so that precise mass conservation is achieved. Without going into details on the transport coefficients needed (these are summarized in Ref 5), Fig. 2 indicates the temperature profiles for an $\mathrm{Al}_{2} \mathrm{O}_{3}$ particle of $30 \mu \mathrm{~m}$ radius and an initial temperature of 2800 K . Particle cooling was driven by Newton's law with constant values of an external environment temperature and heat-transfer coefficient, 500 K and $10^{5} \mathrm{~W} / \mathrm{m}^{2} \cdot \mathrm{~K}$, respectively. We see that $T_{\text {max }}$ at the moment of bubble formation is about 2470 K . Then, from Eq 18:

$$
\begin{equation*}
\sigma \simeq 1.9 \times 10^{-4}\left(T_{\mathrm{cr}}-T_{\max }\right) \simeq 0.5 \mathrm{~N} / \mathrm{m} \tag{Eq19}
\end{equation*}
$$

No data have been found concerning the value of compressibility coefficient $\kappa$ for melted alumina. The values of $\kappa$ given in the literature (e.g., Ref 3) for very different liquids are, in almost all cases, on the order of $10^{-9} \mathrm{~Pa}^{-1}$. This value is used in the present calculations. Possible error in $\kappa$ implies almost the same error in quantities $\Delta R_{\mathrm{s}} / R_{0}$ (given by Eq 11 and 12), which,


Fig. 1 Cross section of a hollow $\mathrm{Al}_{2} \mathrm{O}_{3}+13 \mathrm{TiO}_{2}$ particle. Courtesy of B. Kolman


Fig. 2 Temperature profiles in $30 \mu \mathrm{~m} \mathrm{Al}_{2} \mathrm{O}_{3}$ particle at the times $n \times$ $5 \times 10^{-5} \mathrm{~s}, n=0,1, \ldots, 8$ (solid lines) and cavity surface temperature during solidification (dashed line)
however, remain very small. The value of $R_{\mathrm{b}}^{\min }$ in Eq 8 is much less sensitive to variations in $\kappa$ due to the exponent $1 / 4$.

Let us consider a solidifying alumina droplet with the abovementioned values of $\rho_{\mathrm{m}}, \rho_{\mathrm{s}}, T_{\mathrm{max}}, \sigma, \kappa$, and radius $R_{0}=30 \mu \mathrm{~m}$. The necessary condition ( Eq 11 ) to give rise to a stable bubble is $\Delta R_{\mathrm{s}} / R_{0} \geq 8 \times 10^{-4}$. The sufficient condition (Eq 12) is $\Delta R_{\mathrm{s}} / R_{0} \geq$ $9 \times 10^{-4}$. These two values of the solid shell thickness are almost equal and very small. Consequently, the bubble arises immediately after the start of solidification.

The minimum bubble radius is given by Eq 8 and 9 , $R_{\mathrm{b}}^{\mathrm{mIn}} / R_{0}=1 / 20$. We remark that the pressure of surface tension $2 \sigma / R_{\mathrm{b}}^{\mathrm{min}}$ is about 0.6 MPa , a considerable value.

The velocity driven by the temperature gradient here is:

$$
\begin{equation*}
\mathrm{v} \simeq 1.3 \times 10^{-4} \frac{R_{\mathrm{b}}}{\mu} \operatorname{grad} T \tag{Eq20}
\end{equation*}
$$

In view of the lack of experimental data, we estimate $\mu \simeq(1-$ $10) \times 10^{-3} \mathrm{~kg} / \mathrm{ms}$. The temperature gradient implied by numerical modeling (see Fig. 2) is on the order of $100 \mathrm{~K} / R_{0}$. Then, a bubble of radius $R_{\mathrm{b}}=R_{0} / 10$ moves with velocity $\mathbf{v} \simeq(0.1-1)$ $\mathrm{m} / \mathrm{s}$, a value higher than the velocity of the solid/liquid boundary motion during the process in question (again, see Fig. 2).

According to Eq 17, the final cavity radius is $R_{\mathrm{c}} \simeq 0.67 R_{0}$, a value precisely confirmed in Fig. 2.

## 4. Concluding Remarks

It has been shown that the formation of a cavity in a solidifying drop starts from vapor bubble. The reason is the cavitation phenomenon in response to a pressure decrease that occurs due to the lack of material under the growing solid shell. (The possible reabsorption of a gas has not been considered.) The balance of pressures acting in the melted material and in the bubble ( Eq 6 ) im-
plies the minimum bubble radius ( Eq 8 ), which does not depend on the mass densities- $\rho_{\mathrm{m}}, \rho_{\mathrm{s}}$-of the melted and solid phases.

The following physical picture concerns the stability of solution of Eq 6 with respect to the unknown $R_{\mathrm{b}}$. If the solution $R_{\mathrm{b} 1}<R_{\mathrm{b}}^{\text {min }}$ occurs, the value of $R_{\mathrm{b} 1}$ decreases with an increase of solid shell thickness $\Delta R_{s}$. Simultaneously, the pressure in the liquid phase further decreases. Consequently, this liquid is unstable with respect to nucleating a bubble with the larger radius $R_{\mathrm{b} 2}>R_{\mathrm{b}}^{\mathrm{min}}$. If a new bubble arises, the first bubble collapses under the action of the surface tension. Then, the radius $R_{\mathrm{b} 2}$ increases with the growing shell thickness and the process is stable. This is also the reason why only one cavity can occur.

The necessary (Eq 11) and sufficient (Eq 12) conditions of a stable bubble existence give the minimum thickness of the solid shell at the bubble formation. This shell is very thin, implying that the bubble is born at the very early stage of the droplet solidification.

The motion driven by the surface tension inhomogeneity in a temperature gradient is thermophoretic effect. It can be significant when the bubble arises outside the temperature maximum.

The radii of the resulting cavities ( $R_{c} \simeq 2 R_{0} / 3$ ) calculated from our theory are somewhat larger than those found in experiments (Ref 2). The reason is that the atmospheric pressure can diminish the solidifying particle radius $R_{0}$. This effect should be estimated after the values of necessary material constants are known, namely, the creep behavior of solid alumina at high temperatures.

On the other hand, the experimentally found cavity volume $V_{\mathrm{ce}}$ implies that the value of the particle radius decreases by $\Delta R_{\text {atro }}$ which occurs due to the atmospheric pressure. Comparing $V_{\mathrm{ce}}$ with the theoretical value $V_{\mathrm{c}}$ in Eq 16 and neglecting the dilatation proportional to $\alpha_{v}$ yields the following simple relation:

$$
\frac{\Delta R_{\mathrm{atm}}}{R_{0}} \simeq \frac{V_{\mathrm{c}}-V_{\mathrm{ce}}}{3 V_{\mathrm{c}}}\left(1-\frac{\rho_{\mathrm{m}}}{\rho_{\mathrm{s}}}\right)
$$

For alumina particles, this value is approximately 0.1 or less. Craters (open surface voids) found on some spheroidized particles result from asymmetry of the solid shell formation and the simultaneous action of the atmospheric pressure.

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